TABLE 5

Effect of Temperature on the Extent of Deacidification of Degummed and Dewaxed Rice Bran Oil in Biorefining Proces

ı De	summed and Dewaxed title Dian On in Dioterning 1100
	Condition:
	i) Glycerol—theoretical amount
	ii) Enzyme-10% on the wt of oil
	iii) Pressure—10 mm Hg
	iv) Water-10% on the wt of enzyme

Temperature	Reaction	% FFA	Lovibond color (1 cm cell)	
in C	time in hr	in oil	Y	R
50	1	14.7	_	_
	2	12.0	_	_
	5	8.8	_	_
	7	8.2	_	
	10	7.9	13.4	2.5
70	1	10.8		_
	2	8.5	_	_
	5	4.7	_	_
	7	3.6	_	
	10	3.5	9.0	2.2
80	1	15.1	_	_
	2	14.3	_	_
	5	8.8	_	_
	7	6.9	_	_
	10	5.0	10.0	2.3

TABLE 6
Characteristics of Crude and Refined Rice Bran Oil Samples

	FFA	Unsap.	MG %	DG %	TG %	Lovibond color (1 cm cell)	
						Y	R
Crude rice							
bran oil	30.0	4.0	1.2	12.5	53.3	27.0	4.0
Biorefined							
oil	3.6	2.0	1.3	12.8	80.3	9.0	2.2
Biorefined and alkali refined							
oil^a	0.1	2.0	1.0	12.5	84.0	5.0	0.6

^aRefining factor of the oil is 1.2.

encouraging. The reaction has occurred either between the glycerol used and the FFA or between the DG and the FFA. Quite likely both of the two esterification reactions have taken place simultaneously because the DG content in the crude and the biorefined sample is nearly the same and the TG content in the refined sample is significantly increased.

The combined biorefining and alkali refining process compares well in terms of refining factor and color with the miscella refining process regarding hexane (1) and a hexane-alcohol mixture (2) as shown previously in our laboratory and is by far superior to the combined physical refining and alkali neutralization process investigated by the authors in respect to the refining characteristics. The refining factor includes the total per cent loss of oil from the stages of biorefining and alkali refining divided by the FFA of the crude oil.

The overall results obtained in the present study and the fact that the energy required is much lower compared to other processes can suggest that high FFA rice bran oil can be refined with a high degree of economy by a combination of enzymatic deacidification and alkali neutralization.

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ERRATUM

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